

تحت رعاية معالي رئيس مجلس الوزراء المصري المهندس شريف إسماعيل مؤتمر تحلية المياه الحادي عشر في البلدان العربية UNDER THE PATRONAGE OF THE EGYPTIAN PRIME MINISTER ENGINEER SHERIF ISMAIL 11TH WATER DISALINATION CONFERENCE IN THE ARAB COUNTRIES

18-19 APRIL 2017 • INTERCONTINENTAL CITY STARS - CAIRO - EGYPT

Efficiency improvement and sustainability development in power and desalination industry **Corrado Sommariva MD** generation ILF and member of the board President IDA 2011-2013 President EDS 2004-2006 تنظيم WWW, ARWADEX N متعاونوا الدورات السابقة



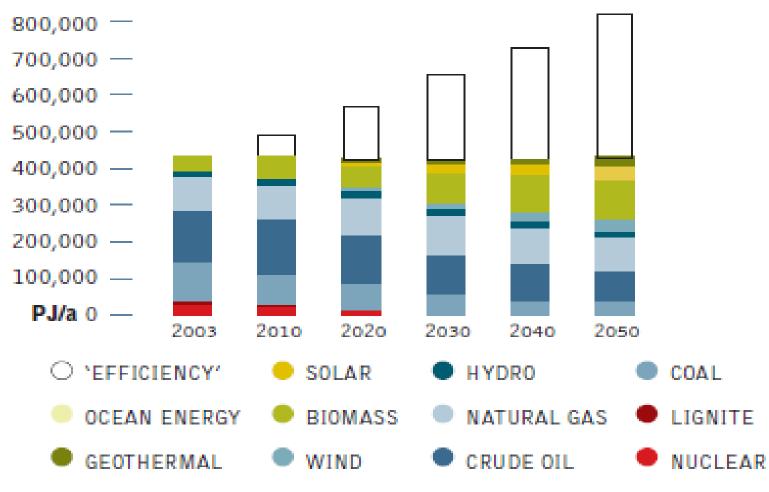
General considerations on efficiency



Half of the climate change problems cold be solved by a smarter use of the existing energy resources

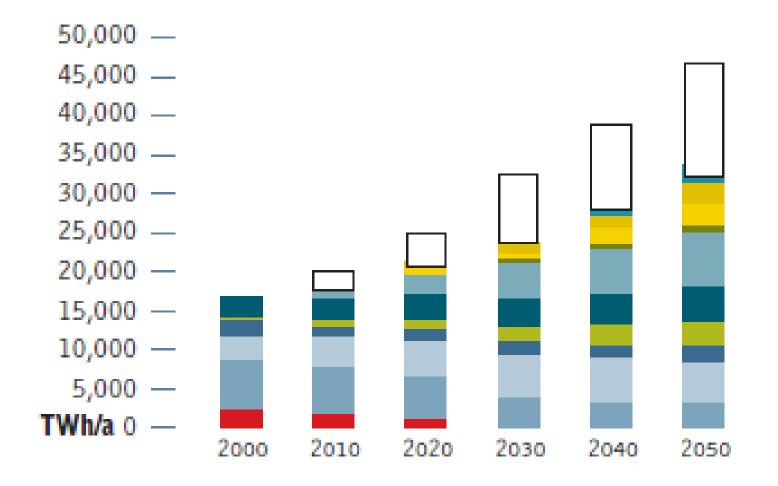


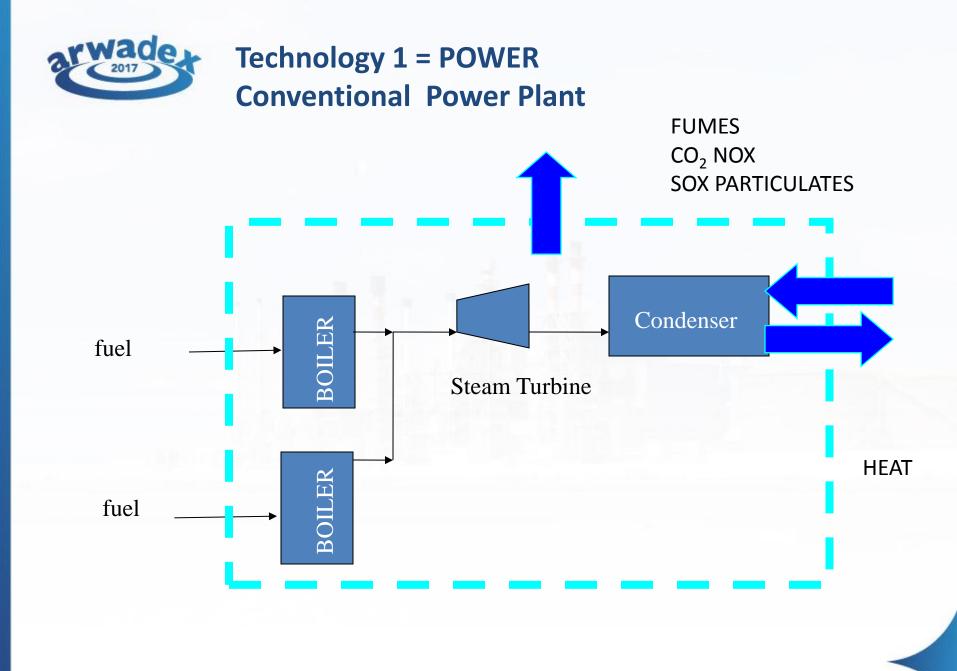
Development of global primary energy consumption under the energy Revolution scenario





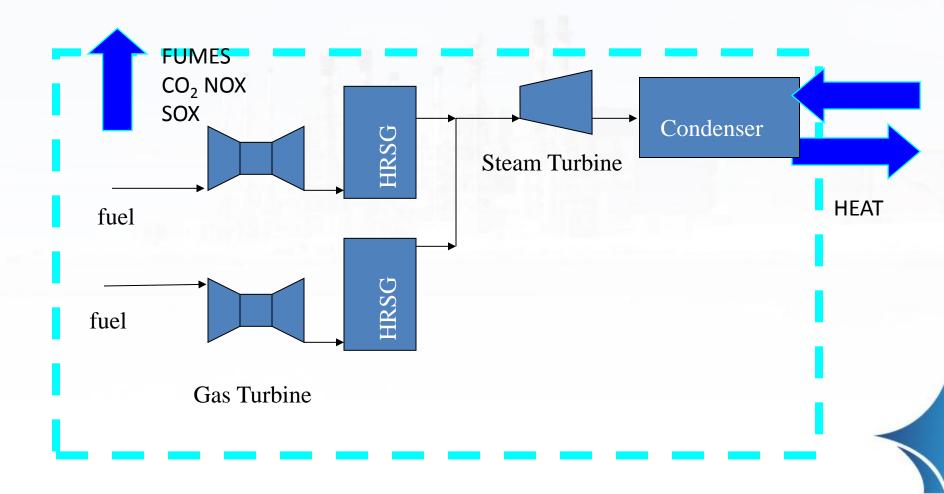
Development of global primary energy consumption under the energy Revolution scenario







Technology 2 POWER CCGT Power Plant - COMBINED CYCLE POWER PLANT





Carnot Efficiency

$\eta_c = \frac{T_E - T_A}{T_E}$

Temperature of the energy supplied

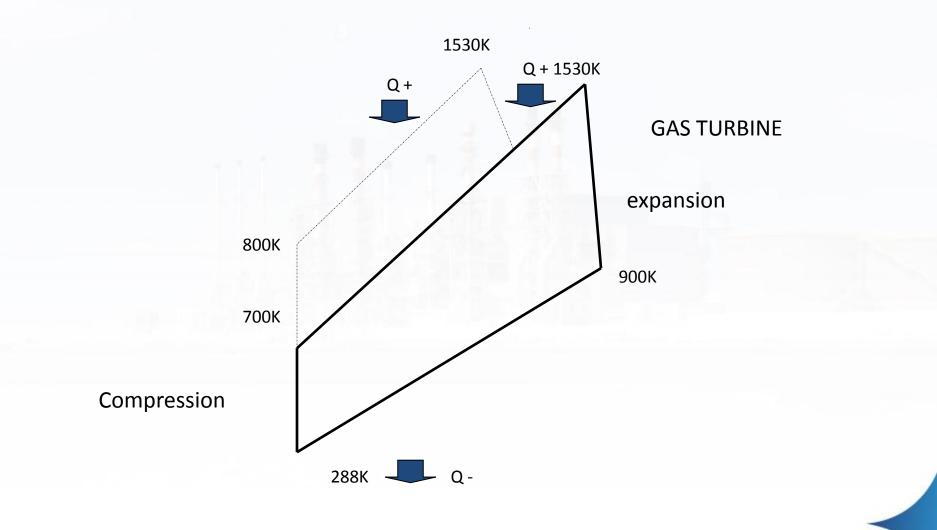
 T_E T_A

Ambient Temperature



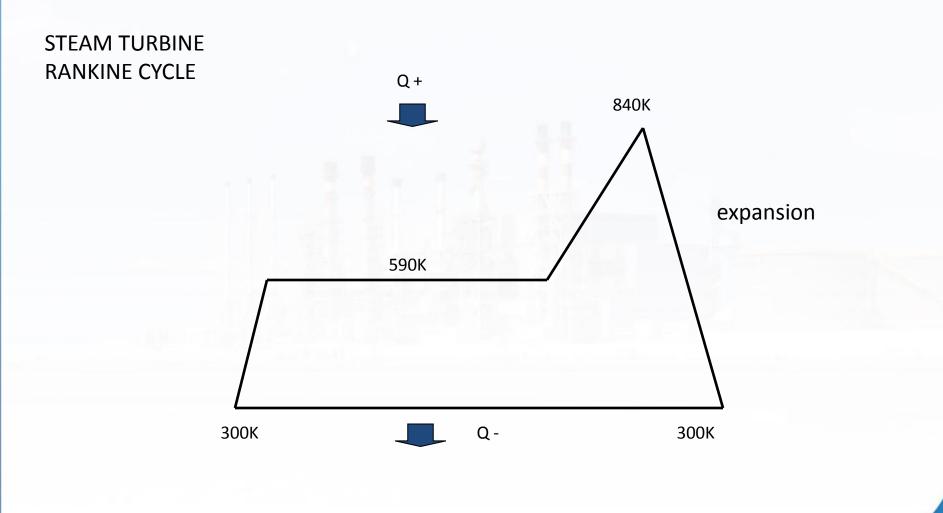


Open cycle Gas Turbine (OCGT)



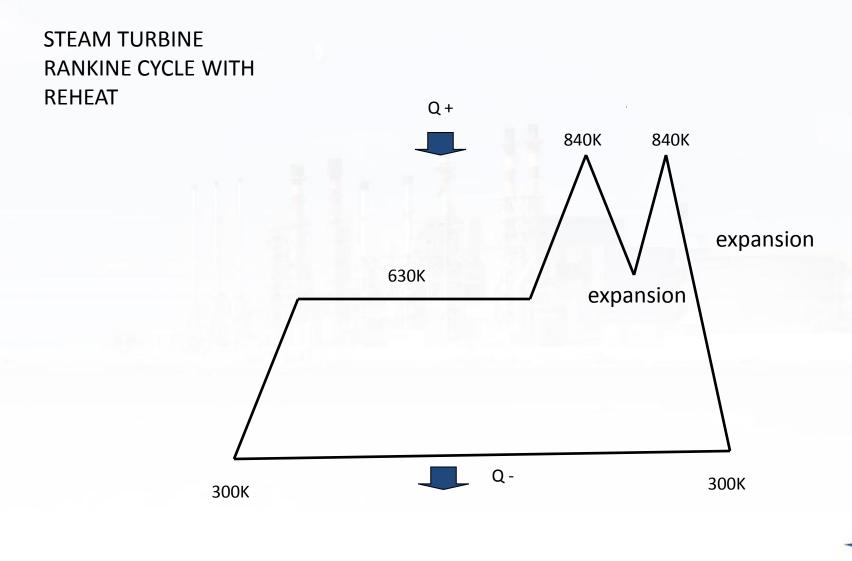


Steam turbine superheat



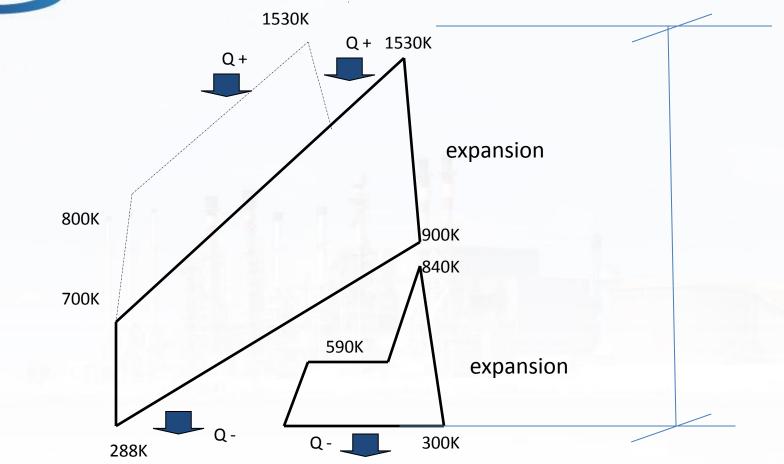


Steam turbine re heat





COMBINED CYCLE



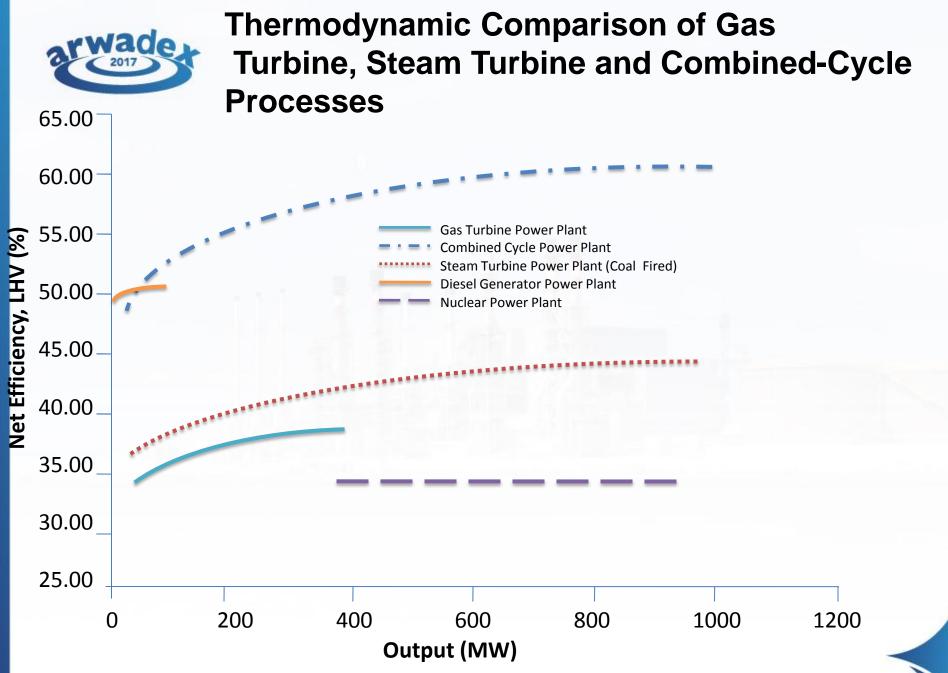




Thermodynamic Comparison of Gas Turbine, Steam Turbine and Combined-Cycle Processes

	GT	ST	CC	
Average temperature of	1,000 - 1,350	640 - 700	1,000 - 1,350	
heat supplied, K (°R)	(1,800 - 2,430)	(1,152 - 1,260)	(1,800 - 2,430)	
Average temperature of	550 - 600	300 - 350	300 - 350	
dissipated heat, K (°R)	(900 - 1,080)	(540 - 630)	(540 - 630)	
Carnot efficiency, %	45 - 50	45 - 57	65 - 78	
GT = Gas Turbine Power Plant,				
ST = Steam Turbine Power Plant,				
CC = Combined-Cycle Power Plant				







Thermodynamic Comparison of Gas Turbine, Steam Turbine and Combined-Cycle Processes



The most environmentally and climate-friendly conventional power plants are combined cycle gas and steam facilities that use natural gas. Such plants have a peak efficiency of more than 58 percent, and their CO_2 emissions per kilowatt-hour (g CO_2/kWh) are only around 345 grams

The corresponding average figures for coal-fired plants worldwide are 30 percent peak efficiency and 1,115 g $CO_{2/}kWh$



Combined cycle Efficiency (gross)

 $= \frac{P_{gt} + P_{st}}{F_{gt} + F_{sf}}$ η_{cc}



power output Gas Turbine

 F_{gt}

fuel input Steam Turbine

 P_{st} power output Steam Turbine

 $F_{_{sf}}$ supplementary firing





Combined cycle Efficiency (net)

 $P_{gt} + P_{st} - P_{Aux}$ η_{ccnet} $F_{gt} + F_{sf}$

power required to run the P_{Aux} power required to ruplant auxiliaries and desalination



Overview of conventional main power and desalination technologies





With power and water generation we have two basic options

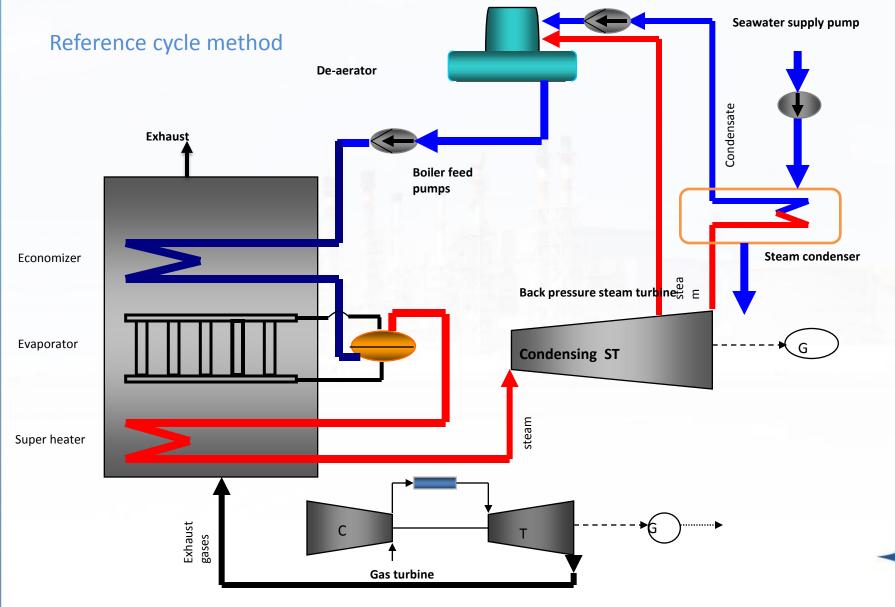
Cogeneration with thermal desalination option 1

Separate power and SWRO desalination option 2

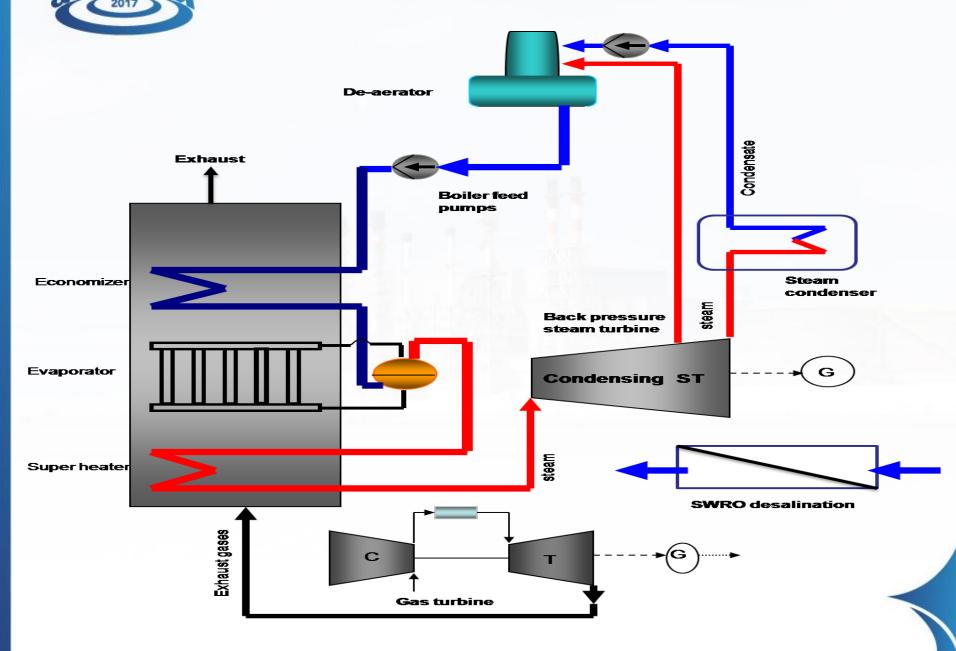




Cogeneration with thermal desalination option 1



ade Separate power and SWRO desalination option 2



Separate power and SWRO desalination option 2









CLASSROOM DISCUSSION

Some example air emissions

CASE 1 600 MW + 40 MIGD

HEAT RATE 8181 KJ/KW hr

FUEL CONSUMPTION 33.6 Kg/s

Equivalent CO2 emissions

4.4 million Tons/yr

10% LOWER air emissions ANYTHING MORE ? **CASE 2** 600 MW + 40 MIGD

HEAT RATE 7387 KJ/KW hr

FUEL CONSUMPTION 30.4 Kg/s

Equivalent CO2 emissions

3.8 millions Tons/yr



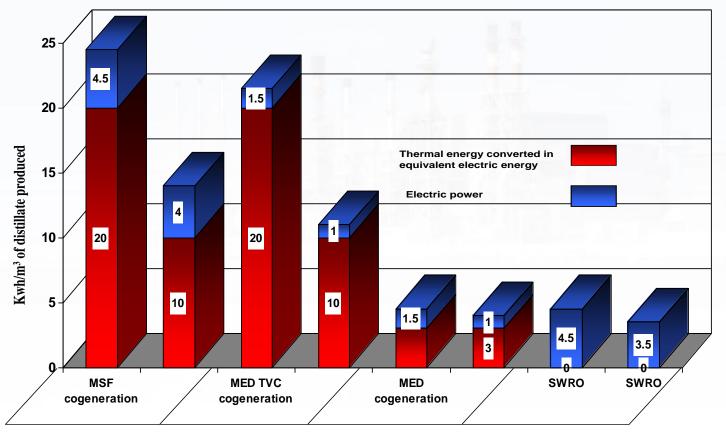


Technologies and efficiency comparison

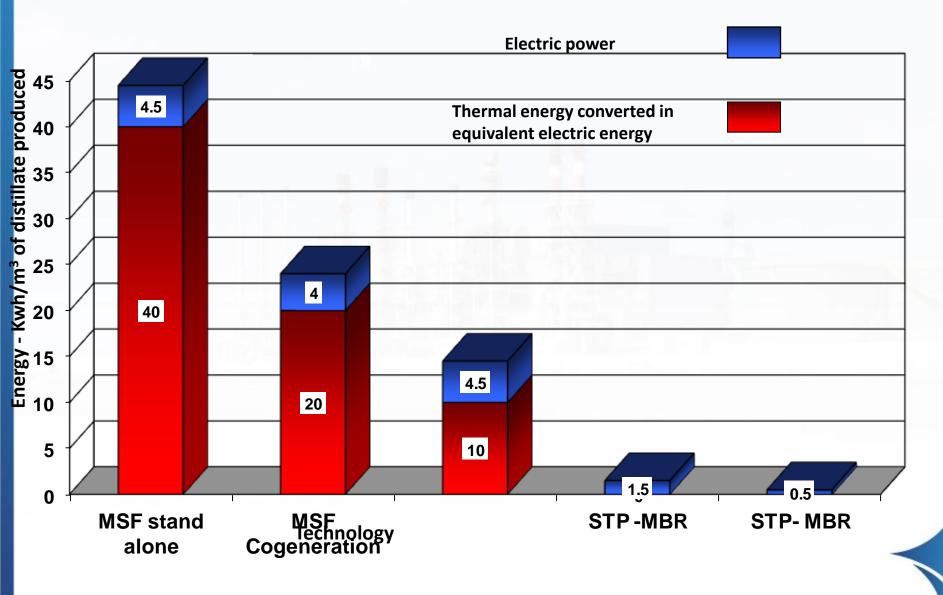


Energy consumption of status of art desalination projects

Desalination plants are very energy intensive processes !!!









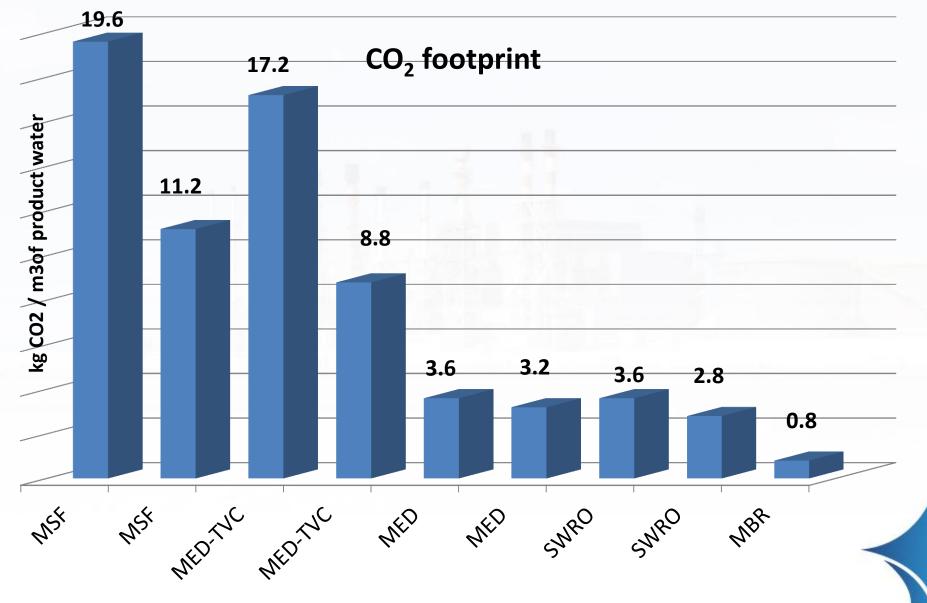
CO₂ footprint

Grid emission Factor

• In parts of the world that are heavily reliant on coal the grid emission factor is somewhere near 0.8TCO₂/MWH.

 Whereas where there is lots of new and efficient system the grid it tends to be lower e.g 0.5TCO₂/MWH







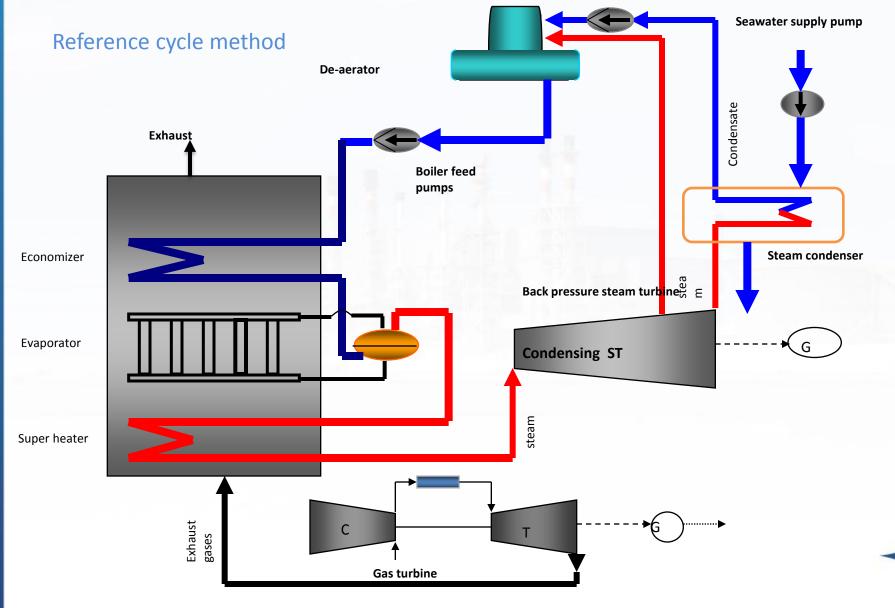
Energy apportionment options

•Energy that could be produced with the steam used for the thermal desalination plant in cogeneration (reference cycle)

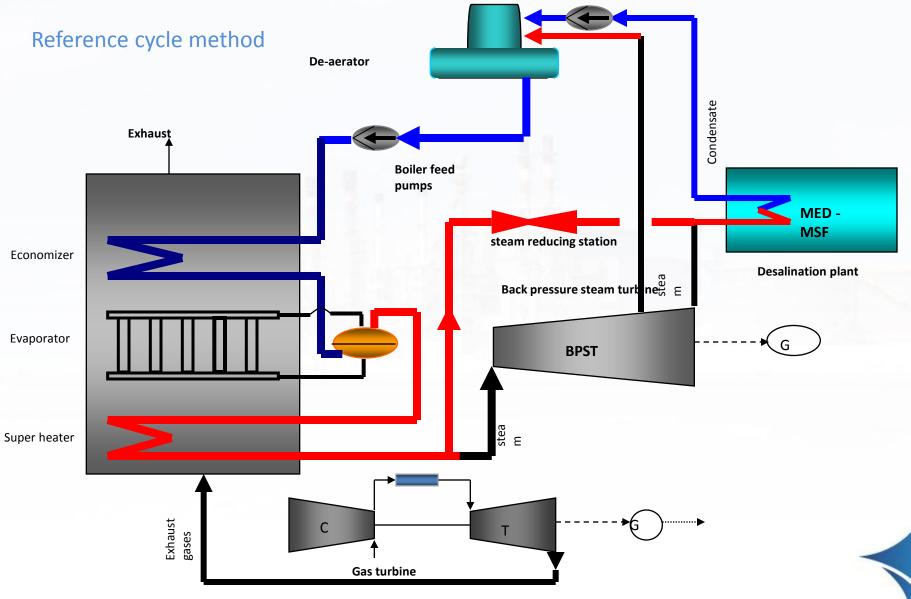
- •Energy required in a stand alone (and that could be produced with the steam)
- •Energy that has been used to produce that amount of steam
- •Energy that could be rendered by the heat at the given temperature

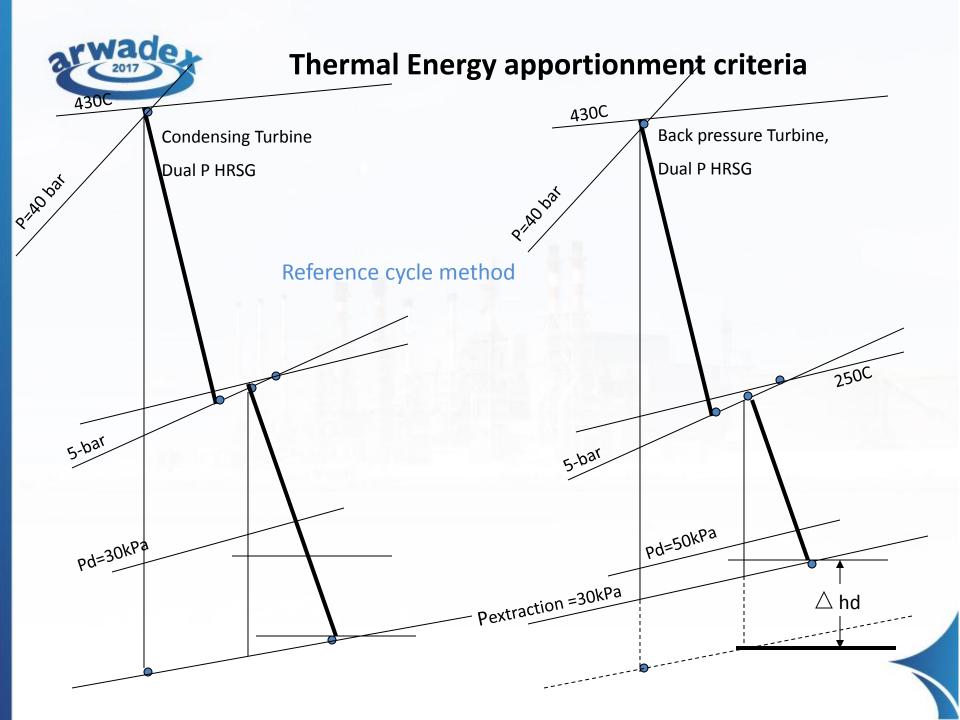










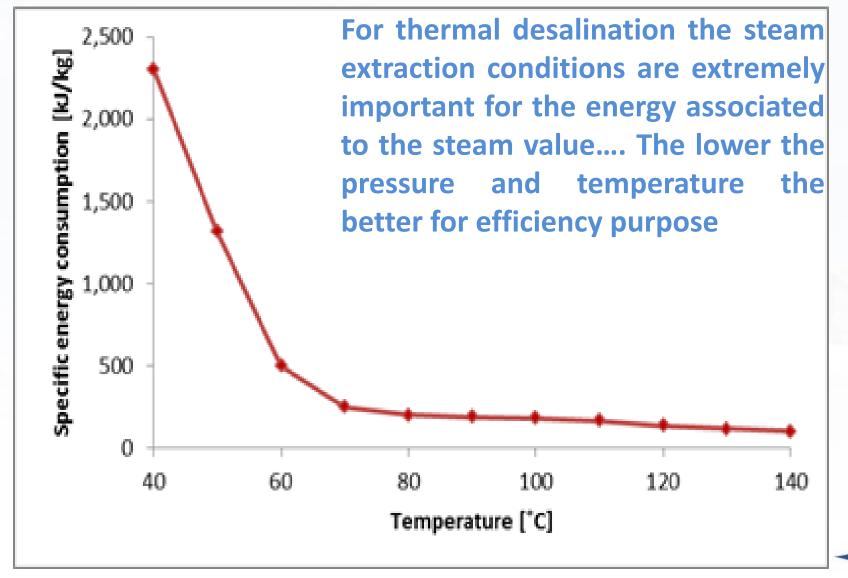




Desalination technologies energy consumption thermal and electric power cogeneration

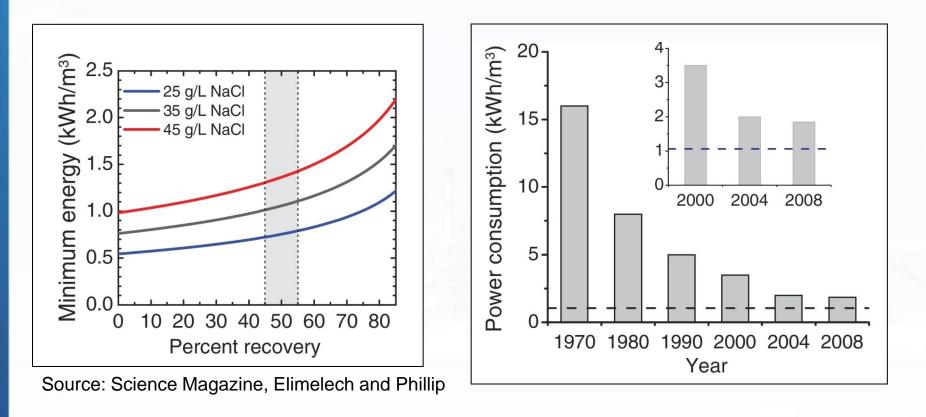
	Specific electric power	Specific heat consumptio n	Steam Extraction pressure	Thermal energy	Equivalent power loss	Total Energy requirements
	Kwh/m ³	kJ/kg	Bar abs	Thermal kwh/m ³	Electric kwh/m ³	kwh/m ³
SWRO (Mediterran ean Sea)	3.5	0	N.A.	0	0	3.5
SWRO (Gulf)	4.5	0	N.A.	0	0	4.5
MSF	4.5	287	2.5-2.2	78	10-20	14-25
MED-TVC	1.0-1.5	287	2.5-2.2	78	10-20	11-21.5
MED	1.0-1.5	250	0.35-0.5	69	3	4-4.5







Theoretical thresholds



Theoretical minimum: 3.5% SW, 50% recovery ~ 1.56 kWh/m³



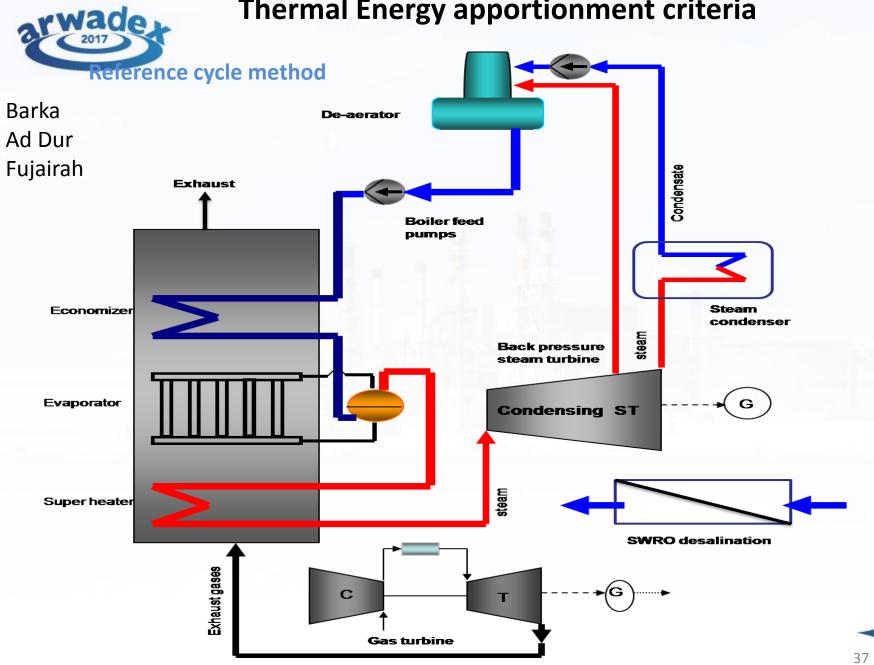
The problem is



 $\Delta H = energy exchanged$ kJ/sec $K_t = overall heat transfer coefficient$ $kJ/m^{2}°C$ A = overall heat transfer area m^2 $\Delta T_{ml} = Delta Temperature (media logarithmic) between the streams °C$

Using low temperature involves a lot of heat transfer..... costs



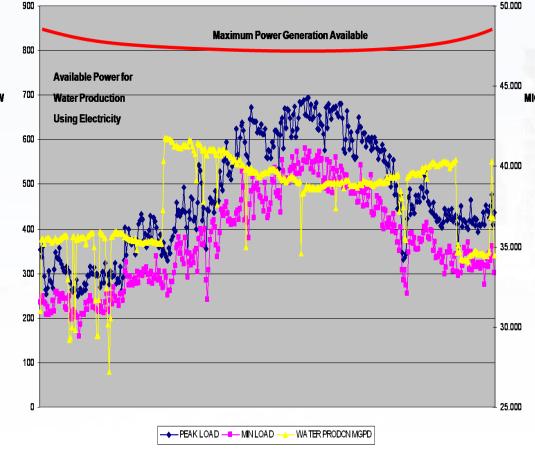


Thermal Energy apportionment criteria

Thermal Energy apportionment criteria



The energy situation



Despite all thermal desalination plant are installed as cogeneration the winter summer unbalance of water and power demand generate tremendous inefficiencies



Data Courtesy of SEWA Layyah Power Plant

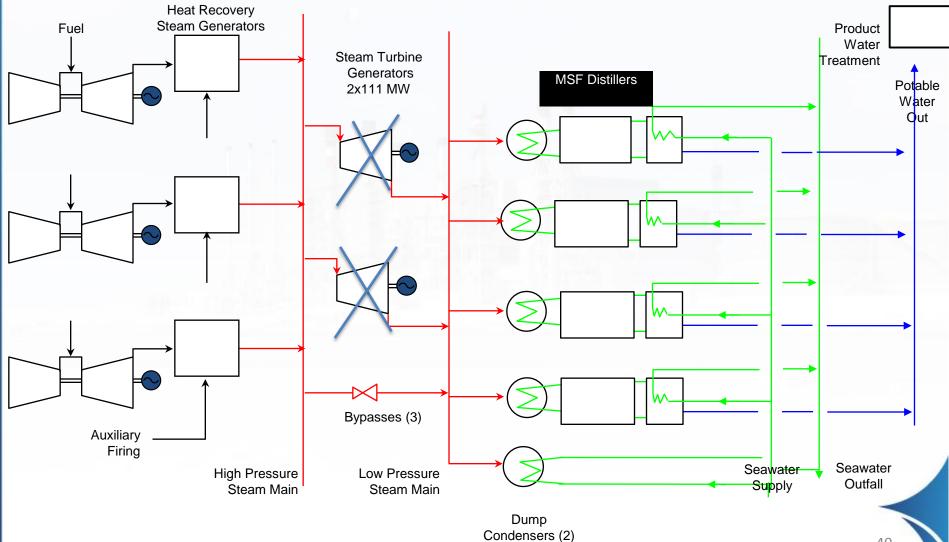
arwader

Thermal Energy apportionment criteria

Since power is no required but water demand keeps almost constant the only solution with thermal desalination is to feed the thermal plant bypassing the steam turbine through steam reducing station

Thermal Energy apportionment criteria

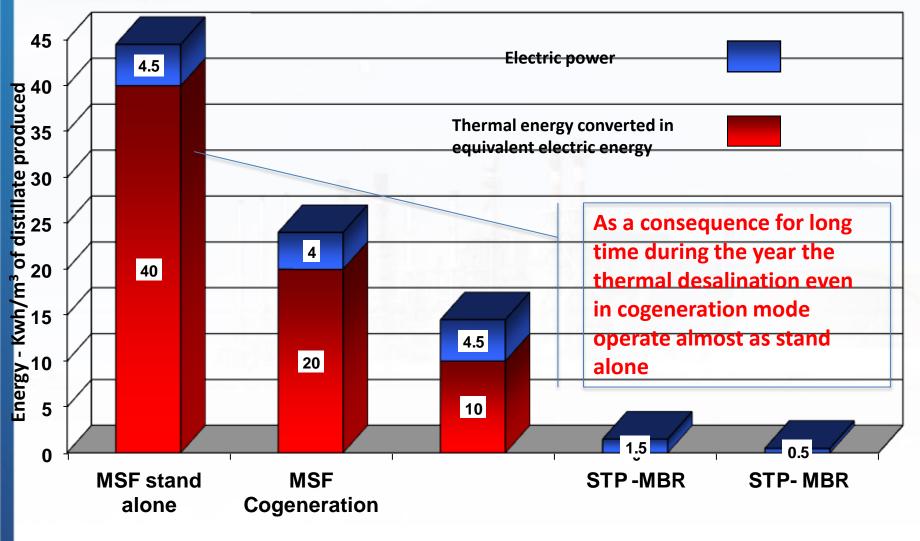
Gas Turbine Generators 3x185 MW (Site Rating)



40



Thermal Energy apportionment criteria





Synergies with WW reclamation to reduce the desal needs and water transmission needs

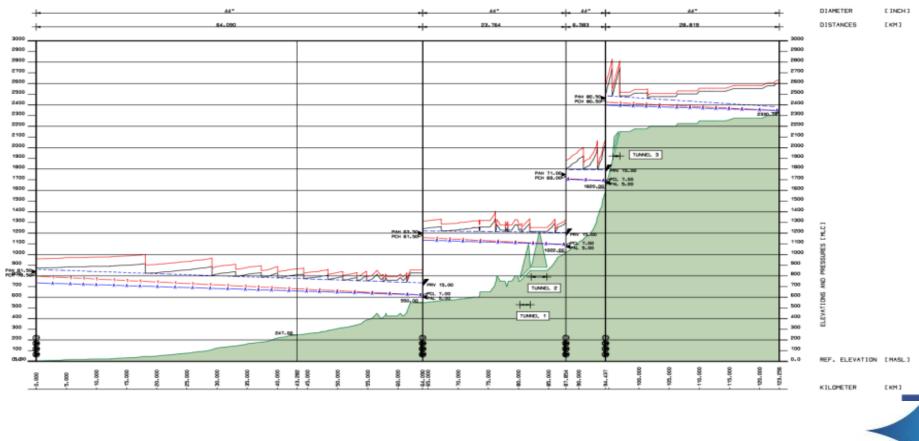
Desalination plant technology	Destination	Generation footprint	Transmission footprint	Total footprint
MSF	East Coast Riyadh	25-30 kWh/m ³	5 kW h/m ³	30-35 kWh/m ³
RO	East Coast Riyadh	7 kW h/m ³	5 kW h/m ³	13 kW h/m ³
MSF	West Coast Abha	25-30 kWh/m ³	10 kW h/m ³	35-40 kW h/m ³
RO	Abha	6kW h/m ³	10 kW h/m ³	16kW h/m ³





Synergies with WW reclamation to reduce the desal needs and water transmission needs

Hydraulic Profile, Shuqaiq – Abha Pipeline

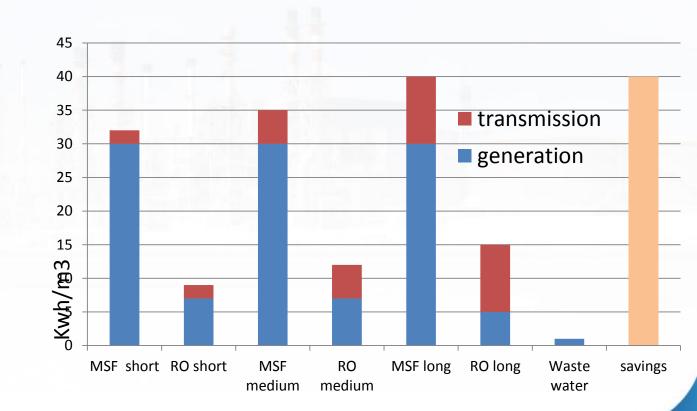




Importance of water re-use for sustainability and energy efficiency

Not only for saving water but most importantly to save energy.

Several large size power generation assets could be saved if this concept was adopted extensively



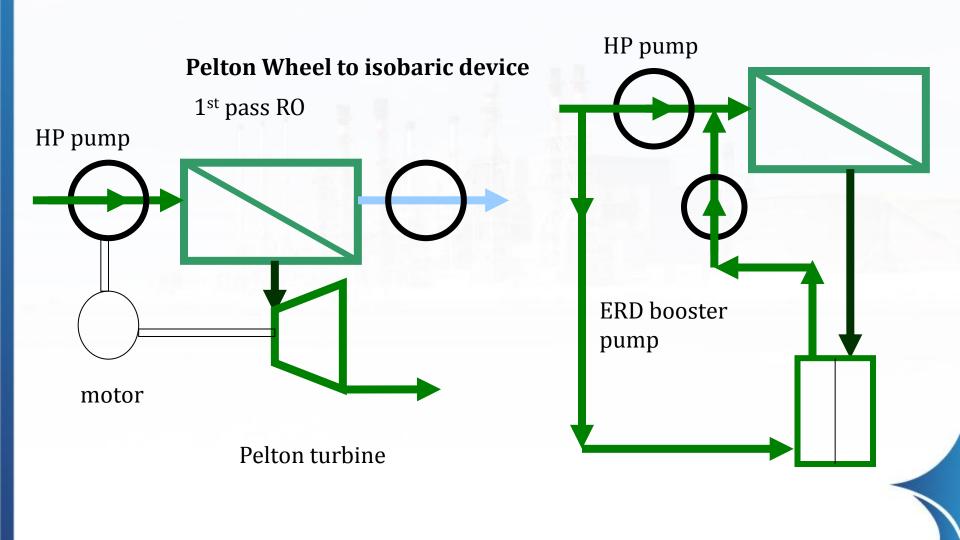




Technology	Thermal	SWRO	Potentials
			Above
Optimization of extraction pressure			2-3 MW per 5 MIGD installed
to the heat input source			
Retrofit of isobaric ERD against			Up to 1 MW per 5 MIGD
traditional Pelton wheel			installed
Retrofit of higher efficiency solution			Depending on the original
for pumping system		10.1	efficiency
Converting brine extraction to			Up to 1 MW per 5 MIGD installed
blowdown extraction			
Redesigning hydraulic circuit for		\checkmark	Extremely high potentials up to 3
major process pump			MW for 5 MIGD installed
			particularly for old operations
Intermediate extraction of Distillate			Depending on the configurations
			up to 0.5 MW per 5 MIGD
			installed
Using MSF/MED drain as feed for			Up to 2 MW per 5 MIGD installed
SWRO			
Others			









Tordera SWRO Plant, Spain. Expansion Retrofit. Original capacity 28,000 m³/d, 4 trains 7,000 m³/d each. Expanded capacity 64,000 m³/d. 4 trains, 16.000 m³/d each Recovery 45%, 15 PX-260 units per train



Before SEC with Pelton wheels: 3.06 KWh/m³

After: 2.56 KWh/m³

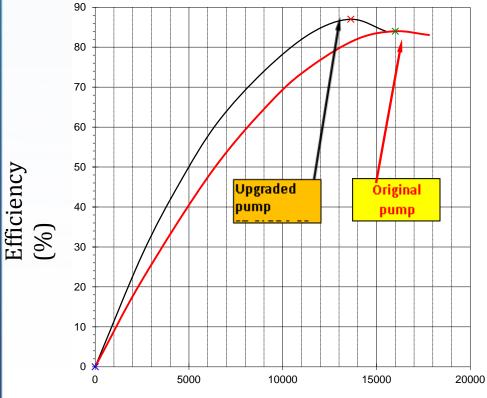
16.3% reduction in SEC



Same HPP, new motor, new membranes in the new trains, same membranes in half of the plant.



Retrofit of higher efficiency solution for pumping system





Al Khobar Power and Desalination Plant, Phase II

Flow (m3/hr)



Efficiency is also in managing your plant !

Poor seawater screening equipment performance bring about and increase in steam condenser pressure



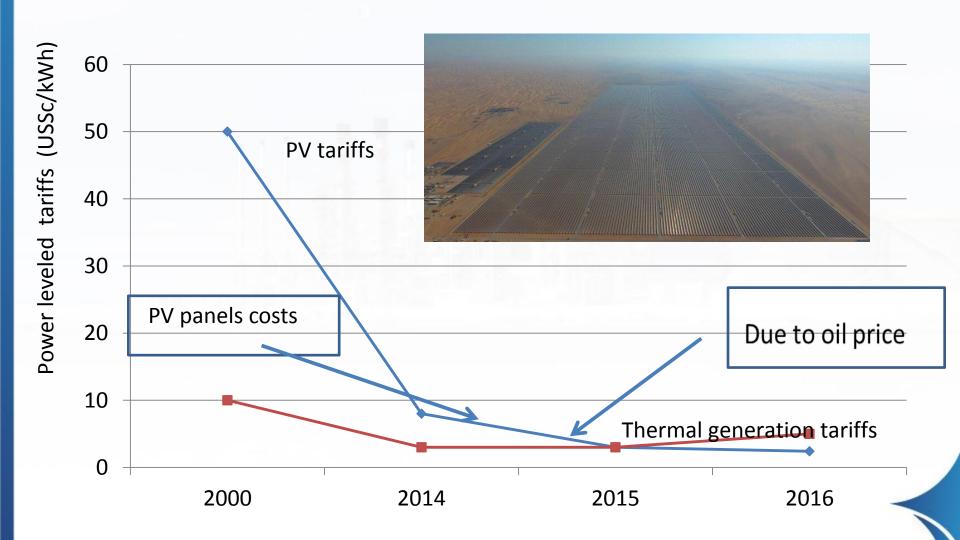


Overview of renewable energy technology and comparison





Evolution of PV system tariff IPP





Evolution of PV system tariff IPP

Renewable energy tariffs				
Year	project	US\$c/kWh		
	Previous pilots- and small installations	20-50		
2014	100 MW SOLAR PHOTOVOLTAIC INDEPENDENT POWER PROJECT - PHASE II	8		
2016	800 MW SOLAR PHOTOVOLTAIC INDEPENDENT POWER PROJECT - PHASE II	3		
2016	350 MW solar photovoltaic plant Shweihan ADWEA	2.4		



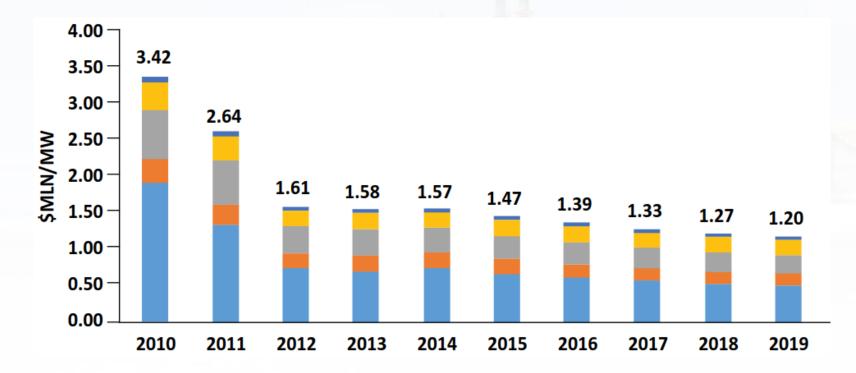
Evolution of PV system tariff IPP

Variables affecting tariffs long			
terms			
Renewables	Thermal power generation		
Land use	Energy costs		
Storage	Land cost		
	New emission limits		
Opportunities	for new tariffs		
Renewables	Thermal power generation		
Better efficiencies	Technology development new more efficient machines		
New installations			



Evolution of PV system

- Significant module Price declines from 2010 to 2020
- Historical Data from more developed markets (Europe, North America, Asia)
- Forecast can be used for other markets for benchmarking purposes





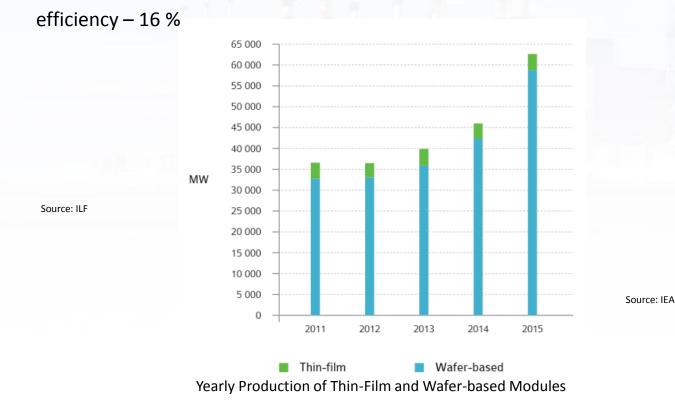
Evolution of PV system Main Developments in Crystalline and Thin Film Technology:

Crystalline: 300 µm

Polycrystalline silicon (p-Si), Monocrystalline silicon (m-Si); high peak efficiency – 21 %

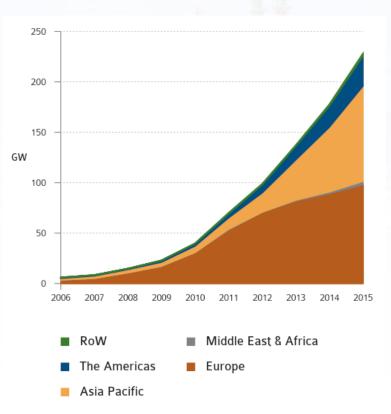
Thin Films: 1 to 3 µm

Amorphus silicon (a-Si), Copper Indium Diselenide (CIS), Cadmium Telluride (CdTe); lower peak





- Installed PV Power until 2015 worldwide: 228GWp
- Strong Increase in Europe and Asia Pacific region in the last 5 years
 - Forecast until 2020: 400GW installed power worldwide

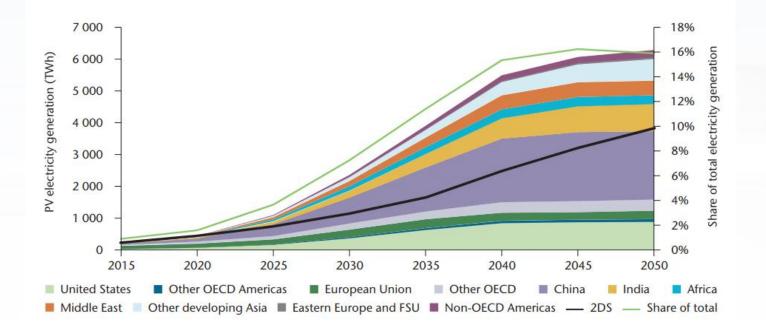




Source: IEA



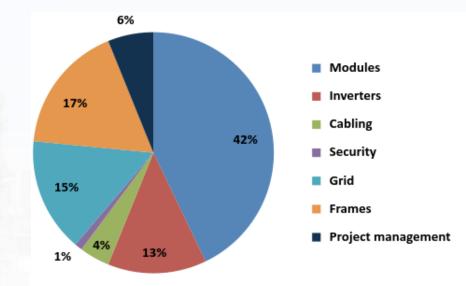
- Forecast for high renewable Energy scenario
 - (Based on 2°C Scenario with high deployment of renewable Energies)
- PV provides 16% of global electricity generation (energy) in 2050







- Average CAPEX costs in 2014: **1.6 million \$/MW** CAPEX and OPEX depend strongly on the considered world region
 - ightarrow High Variation in costs



Variability of CAPEX and OPEX costs observed during 2013 and 2014

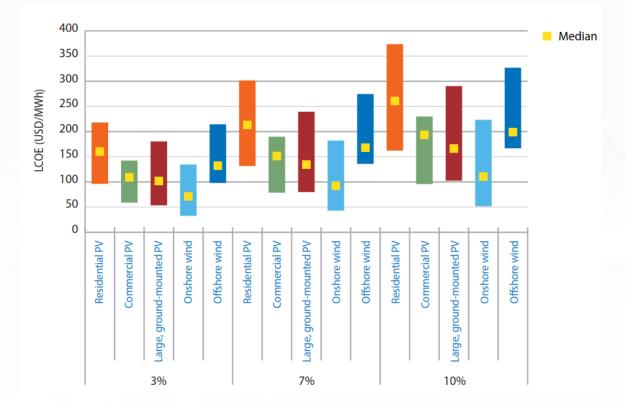




• Comparison of LCOE of different PV and Wind energy systems for different discount

rates

• Medium LCOE for large, ground-mounted PV systems: 100 - 170 USD/MWh



Source: IEA



• Forecast for LCOE based on 2°C Scenario:

Two different scenarios for high and standard deployment of renewable energies

• Global Average for Utility-scale systems:

- 83 USD/MWh for 2DS Scenario

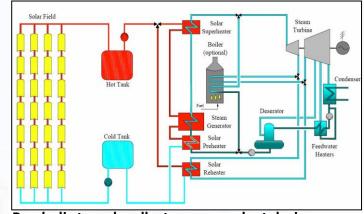
- 75 USD/MWh for 2DS hi-Ren Scenario

Scenario	Technology	LCOE 2015 (USD/MWh)	LCOE 2030 (USD/MWh)	Capacity 2030 (GW)	
2DS	Utility-scale systems	110-294 (164 global average)	68-173 (83 global average)	841	
	Rooftop systems	125-499 (186 global average)	77-389 (110 global average)		
2DS hi-Ren	Utility-scale systems	110-294 (164 global average)	52-129 (75 global average)	1.020	
	Rooftop systems	125-499 (186 global average)	59-214 (94 global average)	1 920	

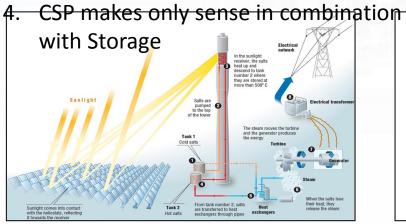
Source: IEA



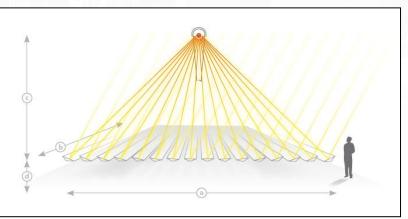
- 1. Parabolic trough systems, most common worldwide
- 2. Solar Tower, highest efficiency
- 3. Linear Fresnel, for industrial applications



Parabolic trough collector power plant design



Solar Tower power plant design

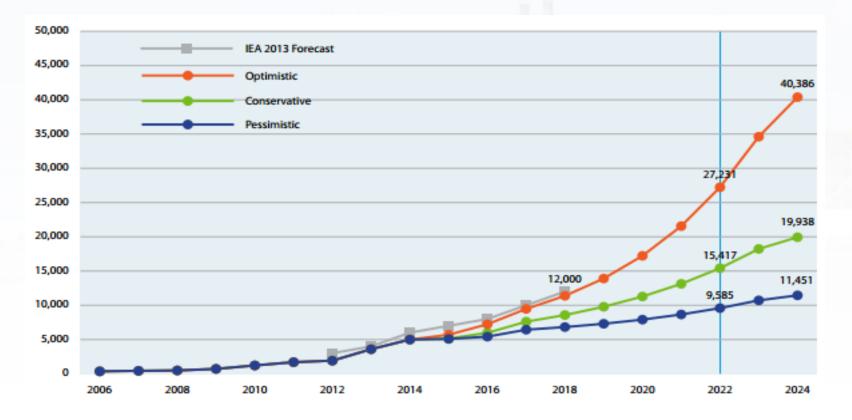


Linear Fresnel system





- Installed PV Power until 2015 worldwide: 5 GWp
- Increase in China, South Africa, Morocco, UEA, India
- Forecast until 2020: 10 GW installed power worldwide

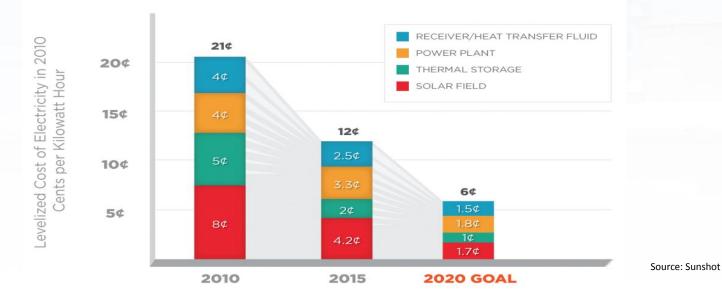




- Average CAPEX costs in 2015 for a Parabolic trough system with 10 h of storage, good DNI around 2400kWh/m²a = approx. 5200 USD / kW
- Average CAPEX costs in 2015 for a SolarTower system with 10 h of storage, good DNI around 2400kWh/m²a = approx. 6000 USD / kW
- Potential reduction of CAPEX for Parabolic trough system until 2020 ~ 6%
- Potential reduction of CAPEX for Solar Tower system until 2020 ~ 32%



- Current LCOE for large scale CSP power plants 2015: 130-210 USD/MWh
- Medium LCOE for large CSP systems in 2020: 80 160 USD/MWh
- Forecast of Sunshot initiative even more agressiv; current offers in Chile for 60 USD / MWh available, UAE is heading towards 80 USD / MWh for 200 MW power plant
- Market is volatile and hardly predictable



The Falling Cost of Concentrating Solar Power



Efficiency by Energy storage



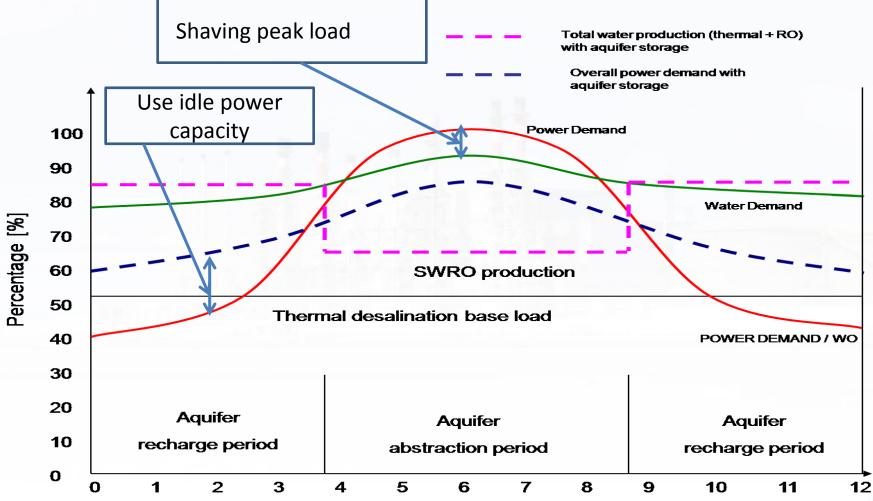


Nuclear and renewable plants must operate at baseload therefore during the Winter months there may not be sufficient electricity generation at co-generation stations to maintain water production of the thermal plants.

A gradual switch of the desalination technology from thermal to SWRO obviously would offer the solution to this problem as SWRO offers the possibility of absorbing part of the idle power load in winter time and can be completely disengaged from the thermal power mode of operation.

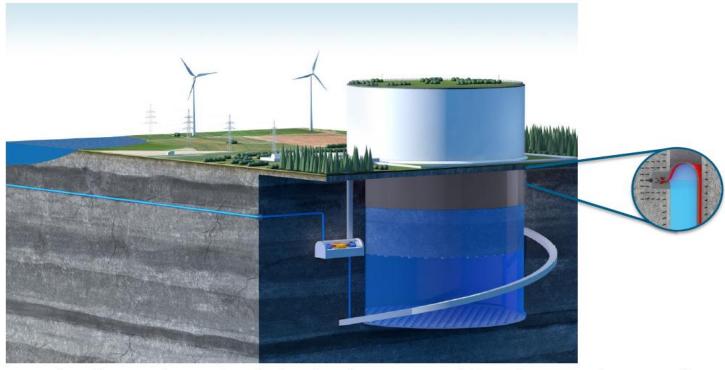


Opportunities for energy optimization





Hydraulic Rock Storage pushes storage of electricity in a new dimension of efficiency

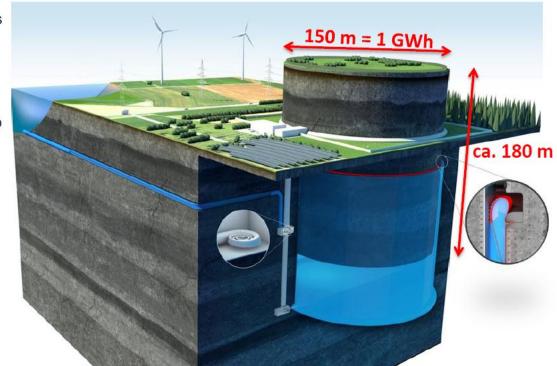


Functionality: A piston of rock that has been exposed from its natural surroundings, is raised up using water pressure, and when power is needed, the water is released and routed to turbines.

The concept of hydraulic hydro storage (HHS) offers an innovative solution because it can store large amounts of energy for a long time.

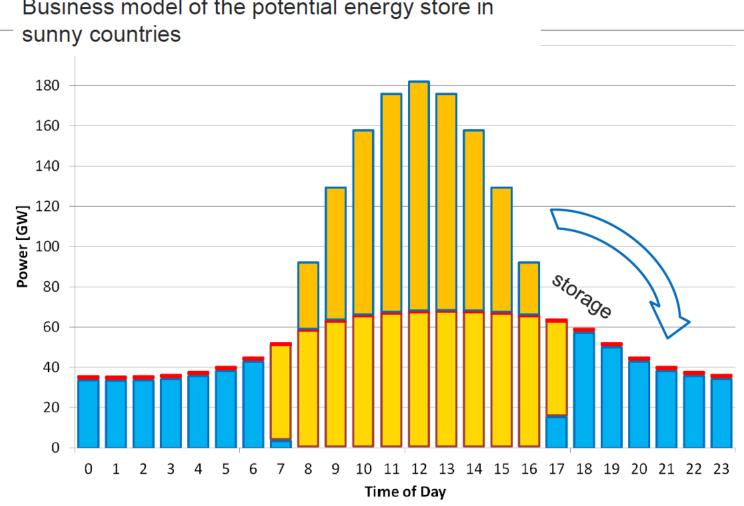


- The rock piston needs to be dismantled from its side walls using rock cutting technology.
- All exposed surfaces will be sealed with geomembranes against environmental impacts and water.
- The piston wears a sealing ring, which is flexible to compensate inaccuracies of the piston wall.
- The storage can be constructed with approved technologies from mining and tunnel constructions.
- 1. Build tunnel to access the bottom
- 2. Separating bottom of piston
- Separating side walls by blasting (parallel to 1, 2)
- 4. Sealing the surfaces
- 5. Installing sealing system
- 6. Installing pumps, turbines and generators etc.









Business model of the potential energy store in



Innovative and advanced desalination technologies and renewable desalination





Advances and new desalination technologies

Thermal		Membrane	
Process	Status	Process	Status
Low energy application to MED technology	Proven in small to medium size pilot plant	Forward Osmosis	Proven in small industrial plant, contracted for new larger applications
LTD desalination	Proven to medium size industrial plant	Biomimetics	Production of initial membranes under further development
Membrane distillation	Proven in small scale pilot	High efficiency membranes	Under further study: laboratory
Forward Osmosis With associated thermal energy for draw solution separation	Proven in small industrial plant, great potentials	Carbon Nanotube	Production of initial membranes under further development
		Pressure Retarded Osmosis (PRO)	Demonstration plant: lab scale
		Carbon Nanotube (CNT)	Production of initial membranes under further development

Advances and new desalination technologies

arwade	
2017	

2017	Thermal			
Process	Energy requirement		Energy optimisation Development outlook	
	Thermal [kJ/kg]	Electric energy [kwh/m ³]	notes	
Low energy application to MED technology	200 Required at 70°C in form of hot water or steam therefore at low exergy value	1.0- 1.5	Relatively limited. However the thermal energy footprint could be reduced to 150 kj/kg.	
LTD desalination	250 kj/kg Required at 70°C down to 50°C in form of hot water or steam	0.8- 3.0 (*)	Potentially very high. However the thermal energy footprint could be reduced to 100 kj/kg.	
Membrane distillation	300-400 kj/kg Required at 70°C down to 50°C in form of hot water or steam	1 - 2.0 (*)	Potentially very high. However the thermal energy footprint could be reduced to 100 kj/kg with multistage installation and proper development of MD membranes	
Forward Osmosis With associated thermal energy for draw solution separation	80-100 kj/kg Required at 90°C in form of hot water or steam	2-3	Specific power consumption development outlook could decrease to 1-1.5 through the development of a dedicated FO membrane	



The Ghantoot experience

- The demonstration includes **5 pilot plants** located in Ghantoot, Abu Dhabi. Each pilot plant will be operated over 18 months;
- Masdar implements the program in **close collaboration** with the Abu Dhabi governmental agencies in the water sector;
- The 5 pilot plants demonstrate different **advanced and innovative** desalination technologies.





The Ghantoot experience

ABENGOA

Abengoa desalination pilot plant







Suez desalination pilot plant



Trevi Systems desalination pilot plant











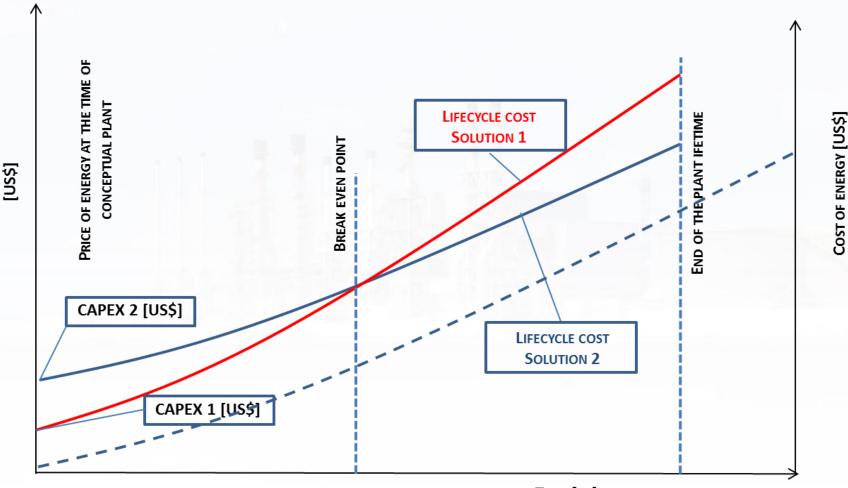


Economics of sustainability and green development

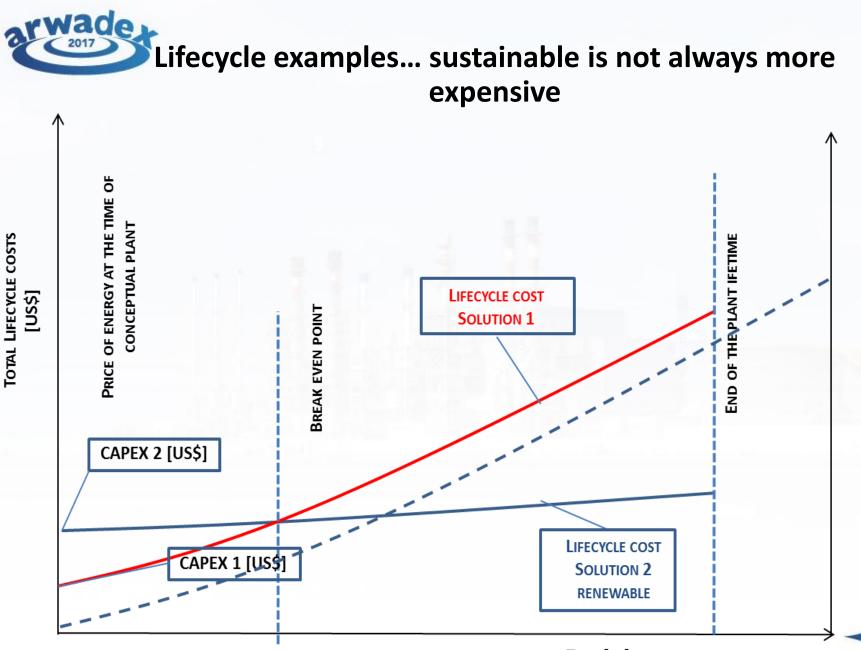




TOTAL LIFECYCLE COSTS



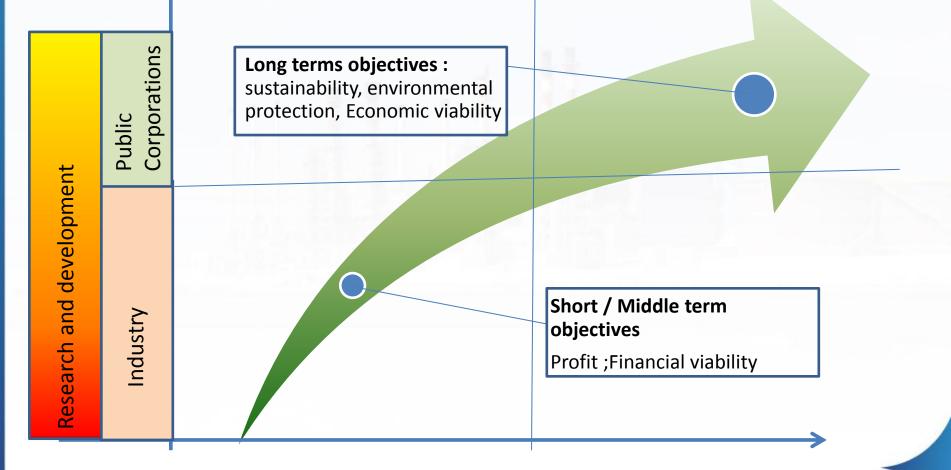
TIME [YR]



COST OF ENERGY [US\$]



Public/ Private Objectives Dichotomy





End of the course

Thanks !!!!!

